



**BC & Yukon Branch**



# Mill Feed Quality: where did all the waste come from?

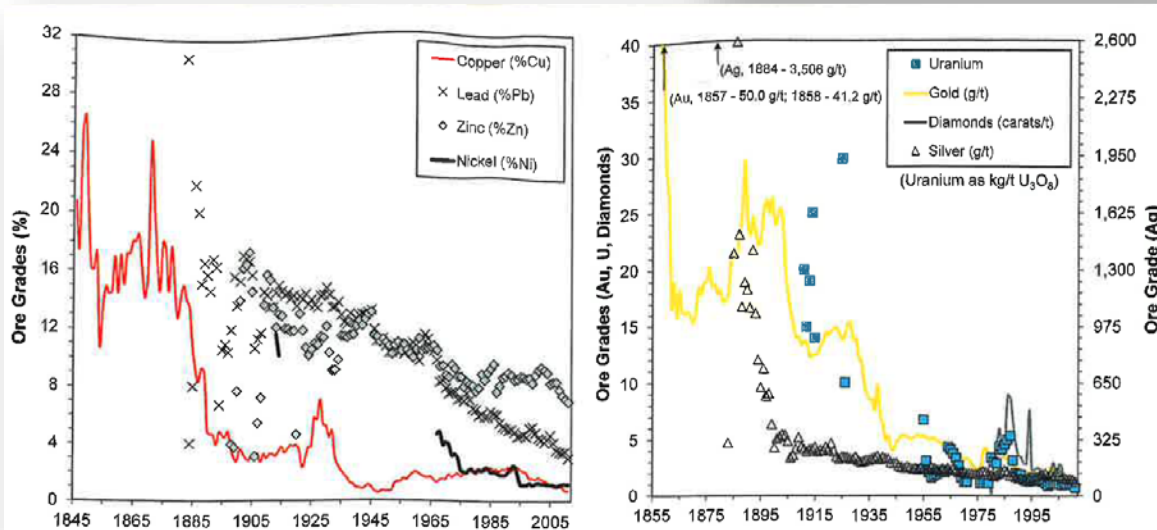
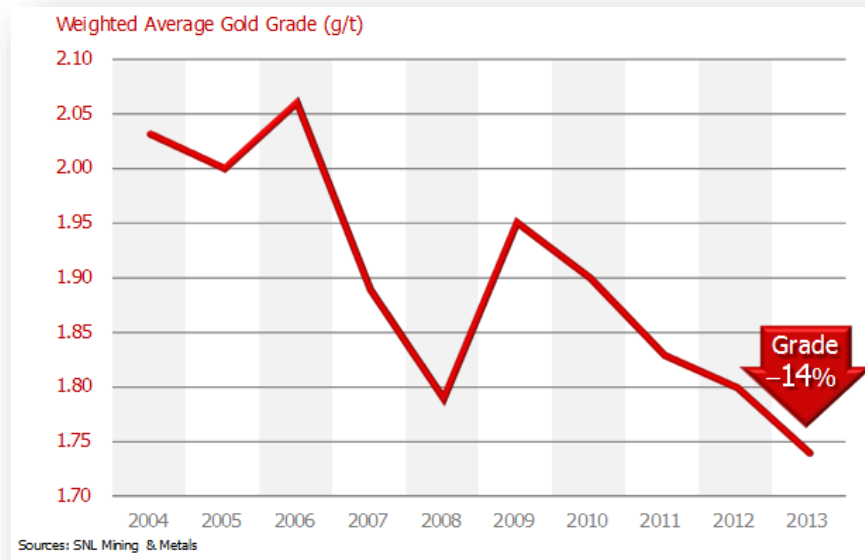
**Adrian Dance & Bob McCarthy**  
SRK Consulting (Canada) Inc.

November 26<sup>th</sup>, 2015

# Mill feed quality issues (1)

## Grade

📉 lower for all metals



# Mill feed quality issues (2)

## Hardness

- ⇒ evident in SAG/AG pebbles

## Complexity

- ⇒ fine-grained
- ⇒ blend of oxide/sulphide minerals
- ⇒ contaminated concentrates
- ⇒ suitable for pre or multi-stage processing options

# Dilution

## Lack of selectivity

- ❧ large, open pit equipment
- ❧ mass underground mining methods

## Internal dilution

- ❧ grade heterogeneity

## Ore vs. waste

- ❧ do they have similar properties?
- ❧ can they be separated?

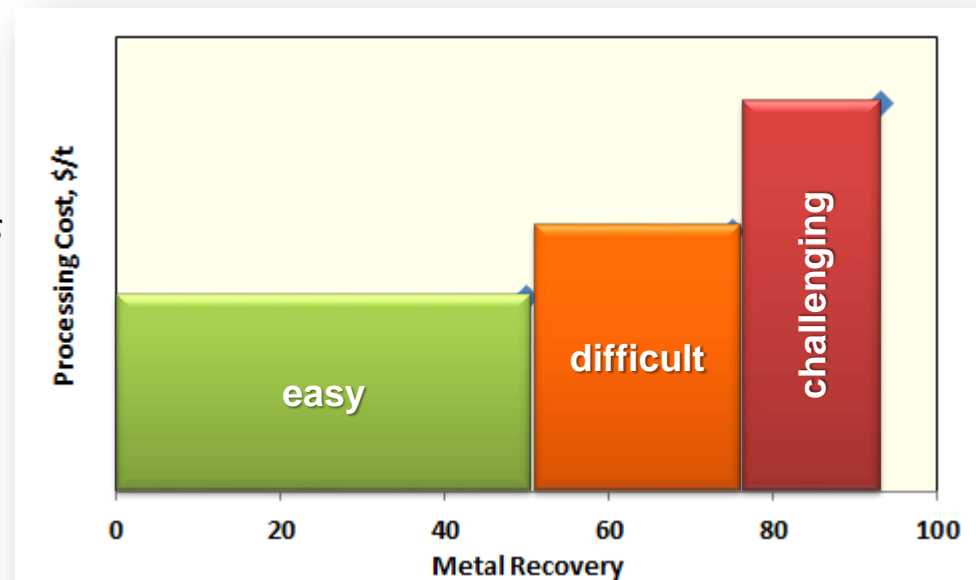


# Opportunities to selectively process?

## Consider mill feed components

- ✦ easy to recover
- ✦ difficult to recover
- ✦ incremental cost?
  - 75% to 85% to 95% recovery
  - finer grind, expensive reagents

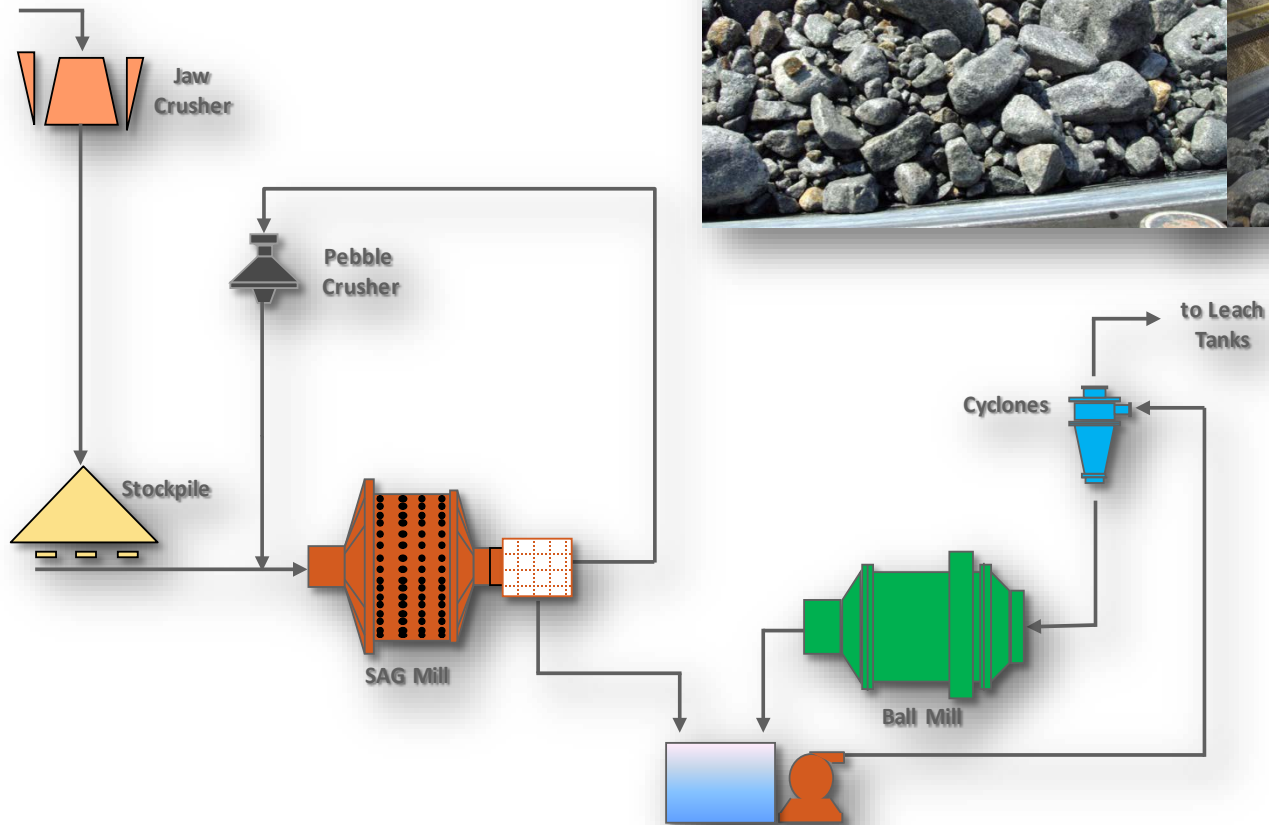
at lower cost  
at higher cost



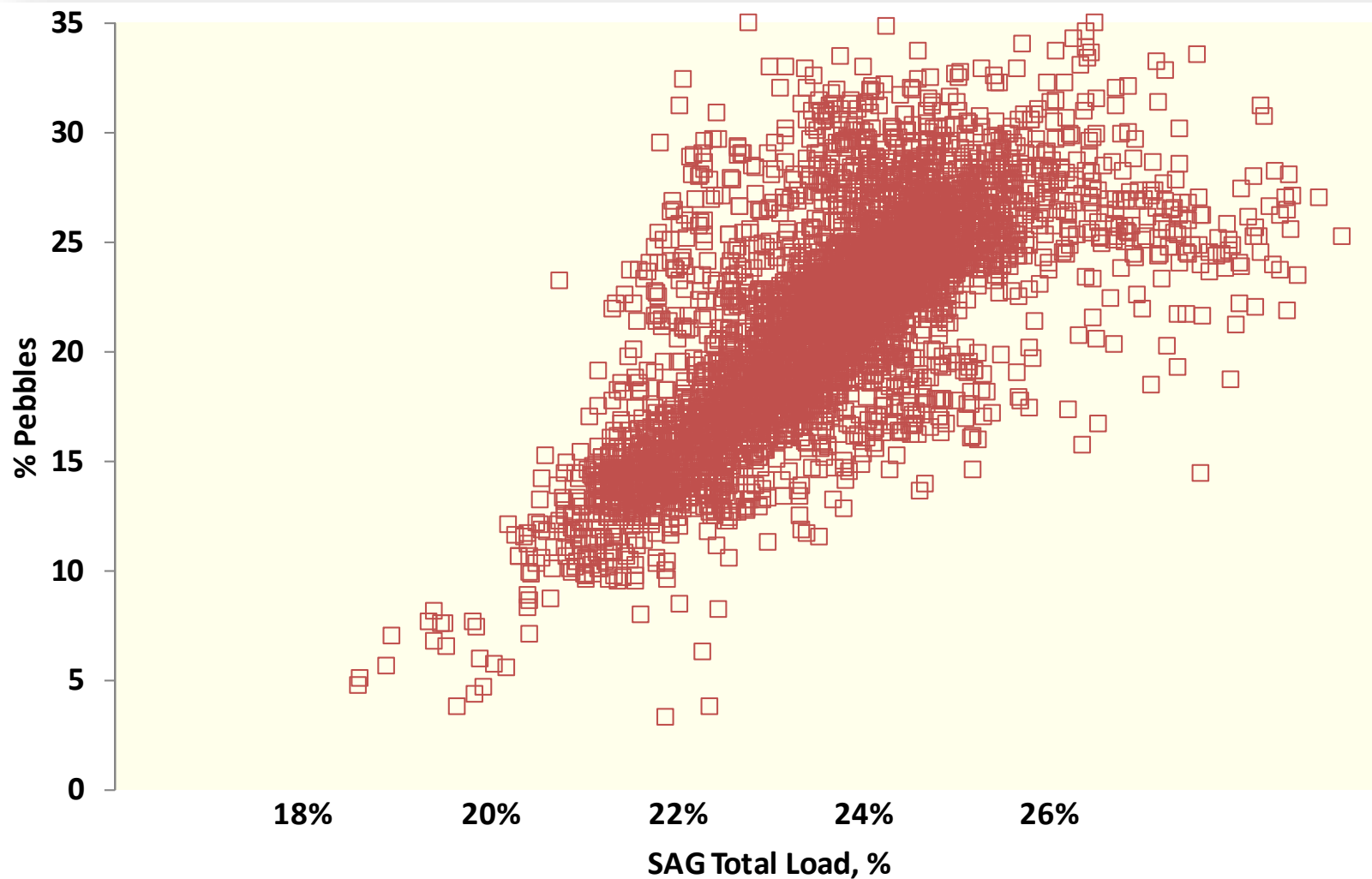
- ✦ each component
  - if isolated, is it 'ore' or should it be subject to a higher cut-off?
- ✦ for example
  - coarse material after blasting & primary crushing

# AG/SAG mill pebbles (1)

Are they worth returning?



## AG/SAG mill pebbles (2)



# Effect of pebbles (1)

## On competent feed

- ⇒ % pebbles proportional to load
- ⇒ up to... “1 tph pebbles  $\equiv$  1 tph fresh”

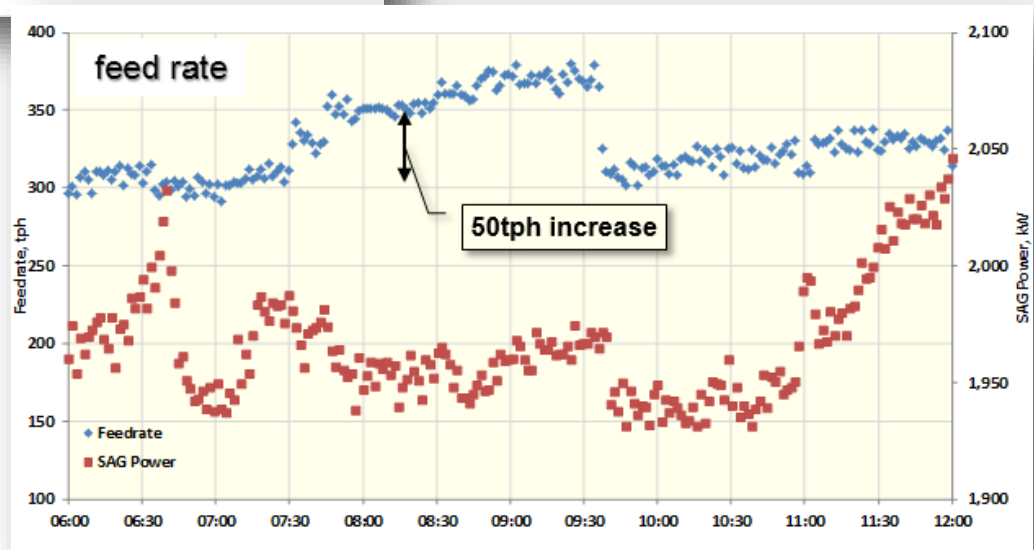
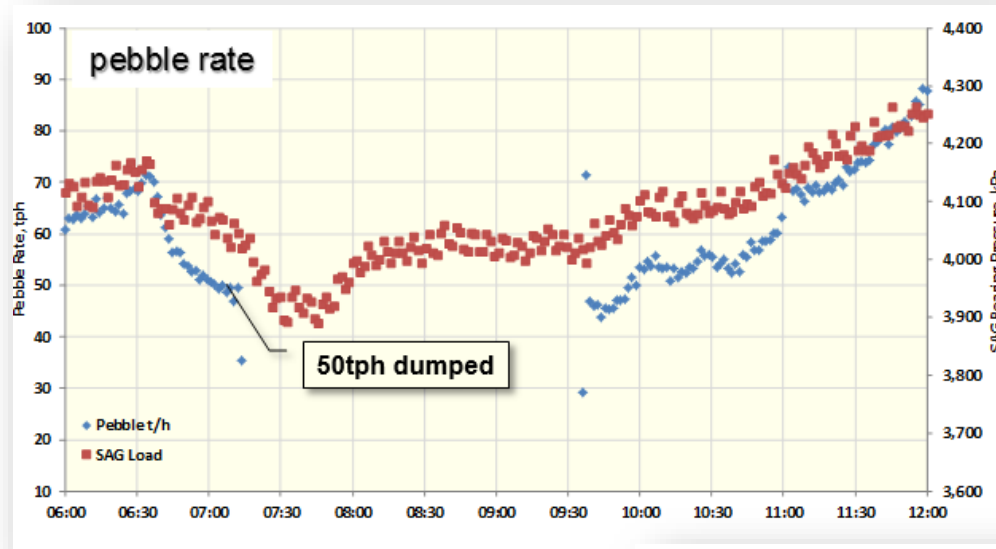
## Pebble distribution

- ⇒ very little broken material
- ⇒ well rounded, coarse pebbles





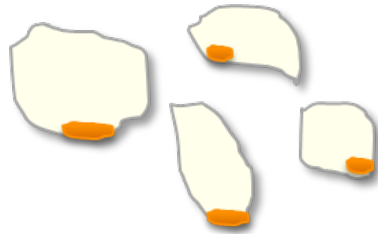
# Effect of pebbles (2)



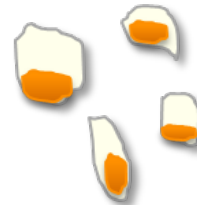
# 'Coarse Beneficiation'... exploiting a natural tendency

## Classification by size

- ☞ preferential grade by size department



coarse >75mm



medium >25mm



fine <25mm

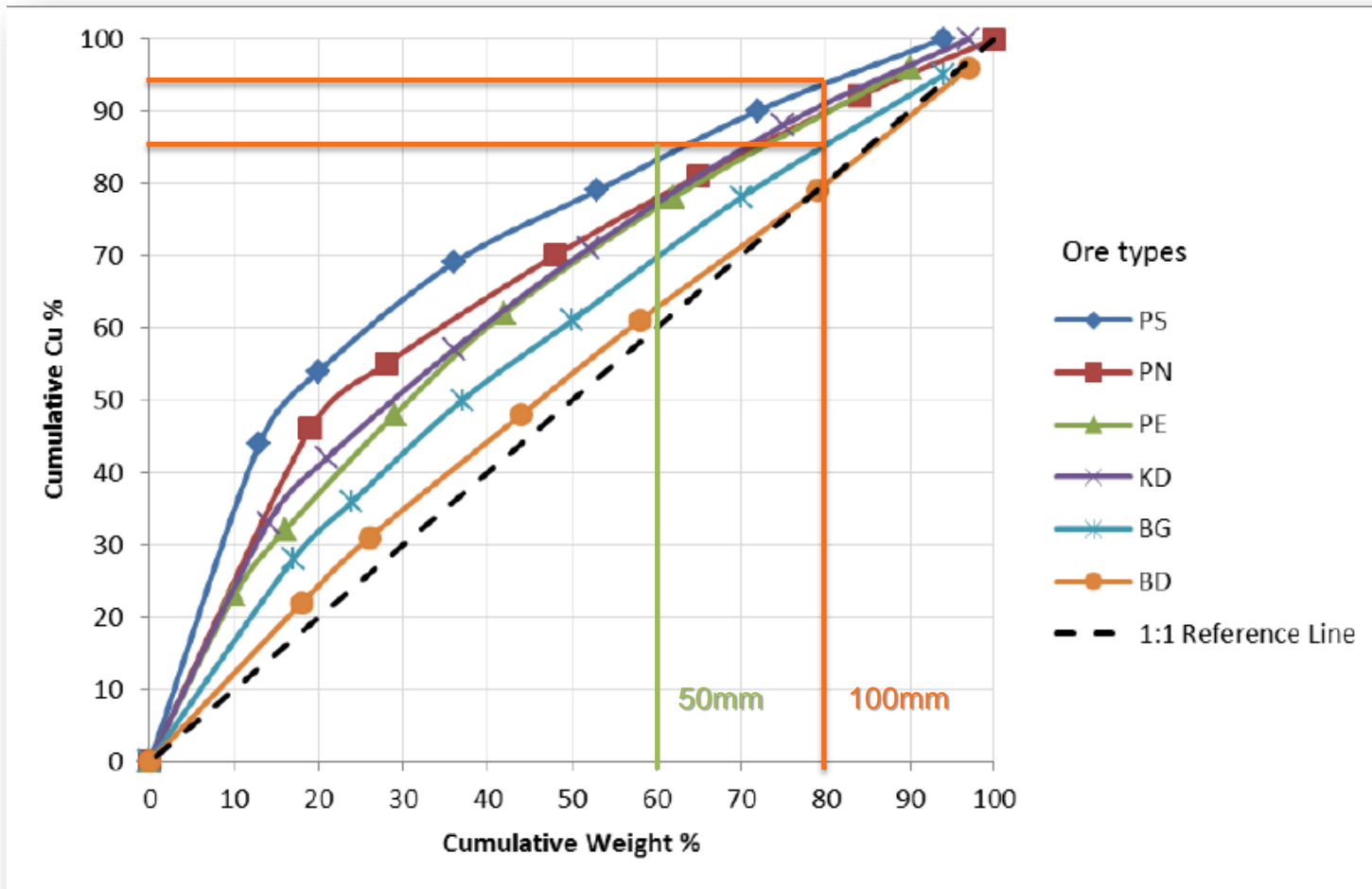
## After two applications of energy...

- ☞ why recombine **competent, coarse** material with **softer, fine** material?
- ☞ coarse material requires higher kWh/t to process
- ☞ competent material should be evaluated at a higher cut-off grade



# Metal vs. size distribution

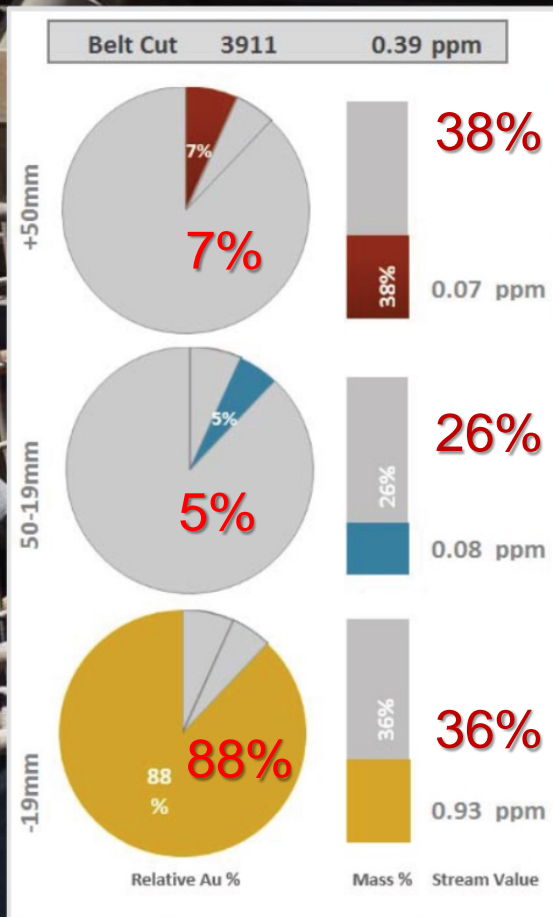
## Bougainville Copper 1986



"The Application of Pre-concentration by Screening at Bougainville Copper Limited", Burns, R., Grimes, A., 1986.

# “Grade Engineering”<sup>®</sup>

(CRC ORE)



## Grade by Size Au Example

An extensive belt-scale sampling program of a gold operation indicated significant grade by size response. Three screened size fractions show major preferential department of Au during blasting and crushing.

Pie diagrams represent %Au and the bar charts represent %mass. In this case 64% of the feed mass contains Au well below economic cut-off. 88% of Au is contained in 36% of the mass below 19mm.

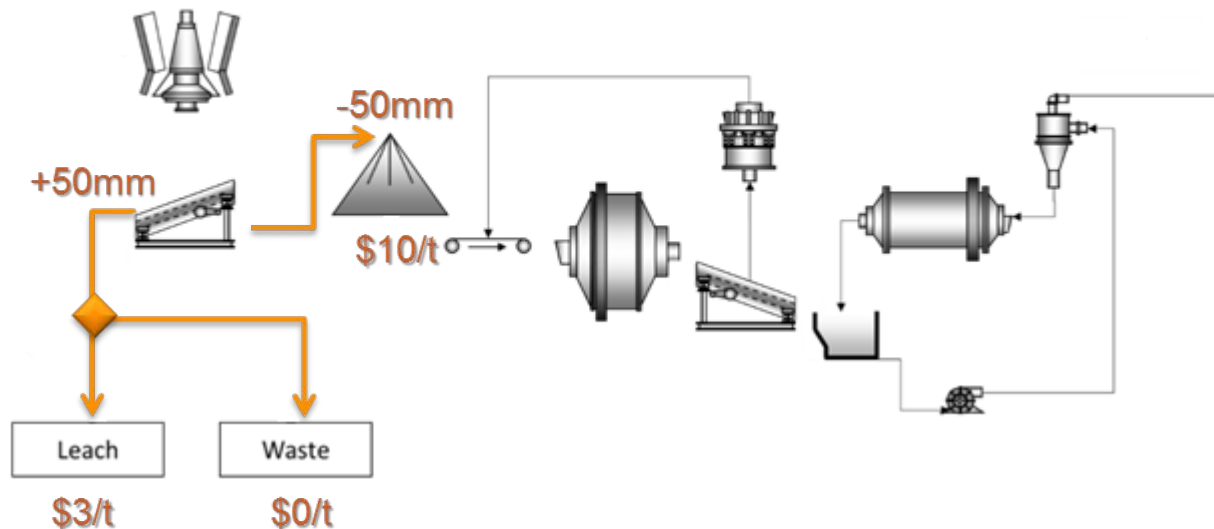
This is not a result of 'dilution'. The in-situ feed grade represents current resource definition practice.

**Grade by size data is typically not collected as a processing attribute.**

# Deferring difficult material

## Coarse screening

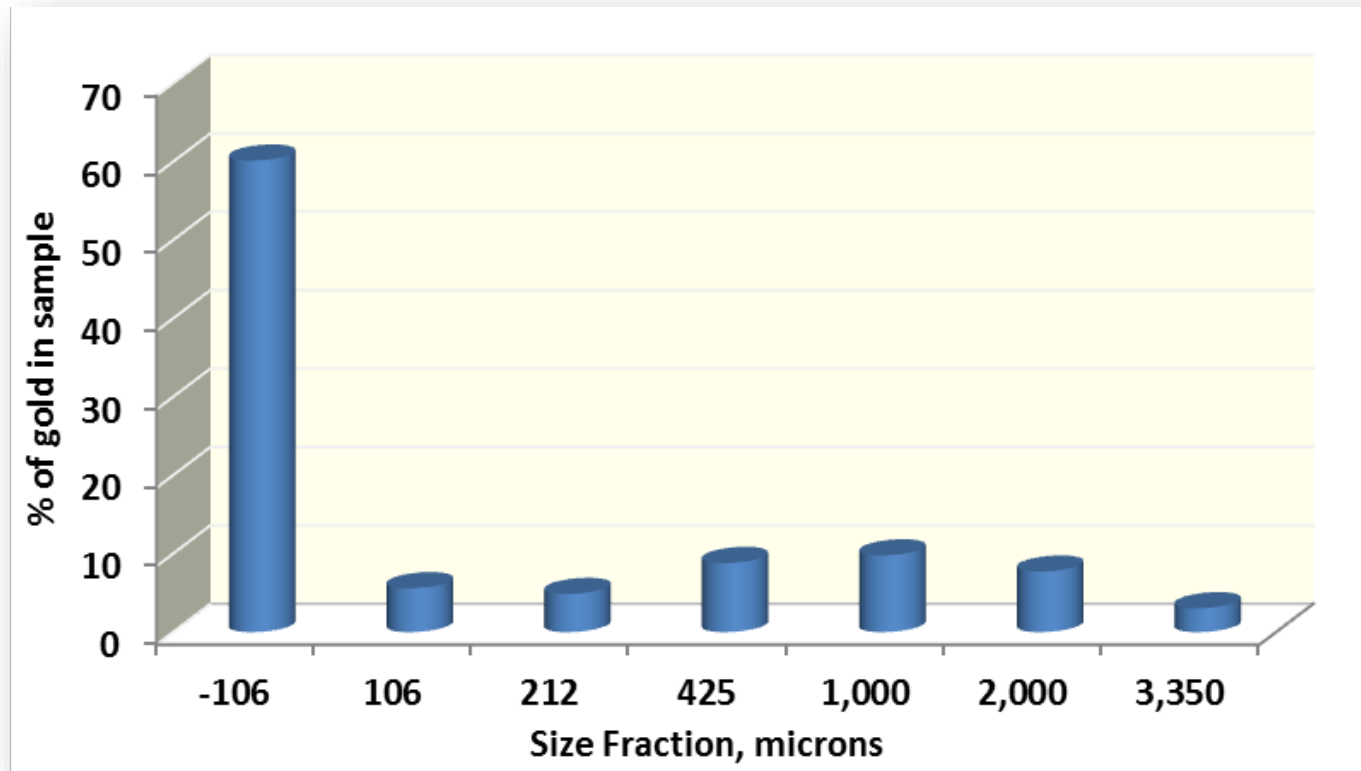
- ≡ eliminate competent component
- ≡ increase mill throughput (lower kWh/t)
  - 15% to 20% higher tonnage
- ≡ possibly lower grade
  - suitable for cheaper processing options



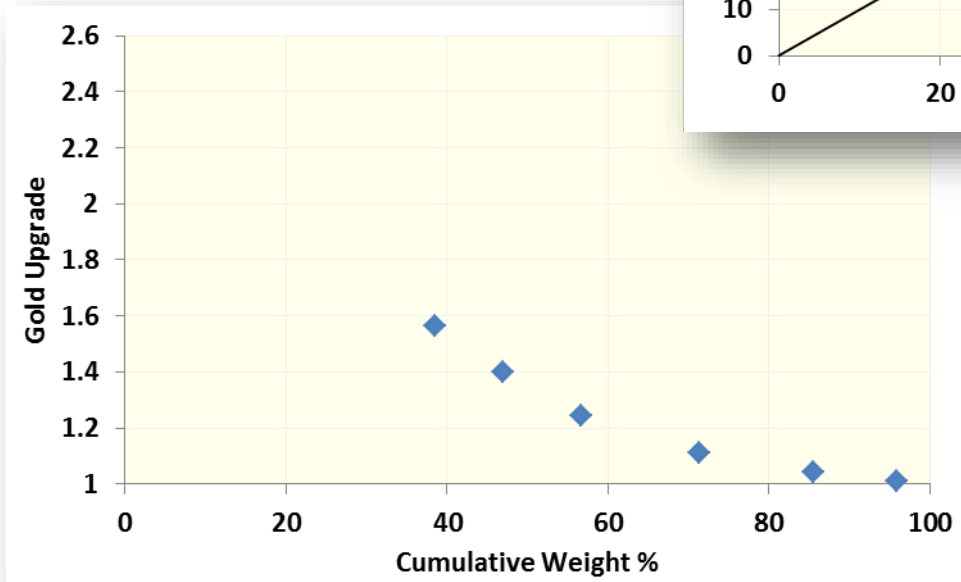
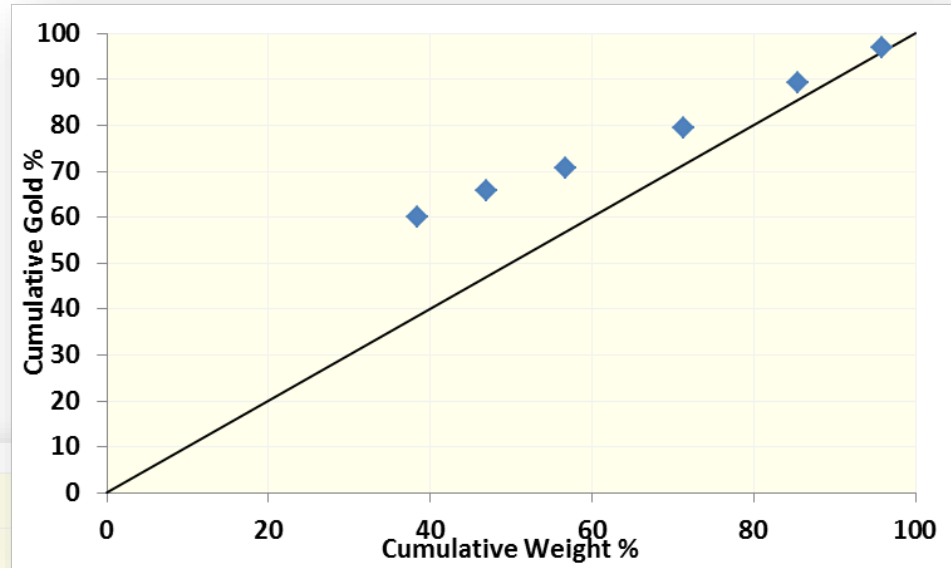
# Challenge...how to assess based on drillcore?



# Example drillcore test results (1)



# Example drillcore test results (2)





# Example drillcore test results (3)

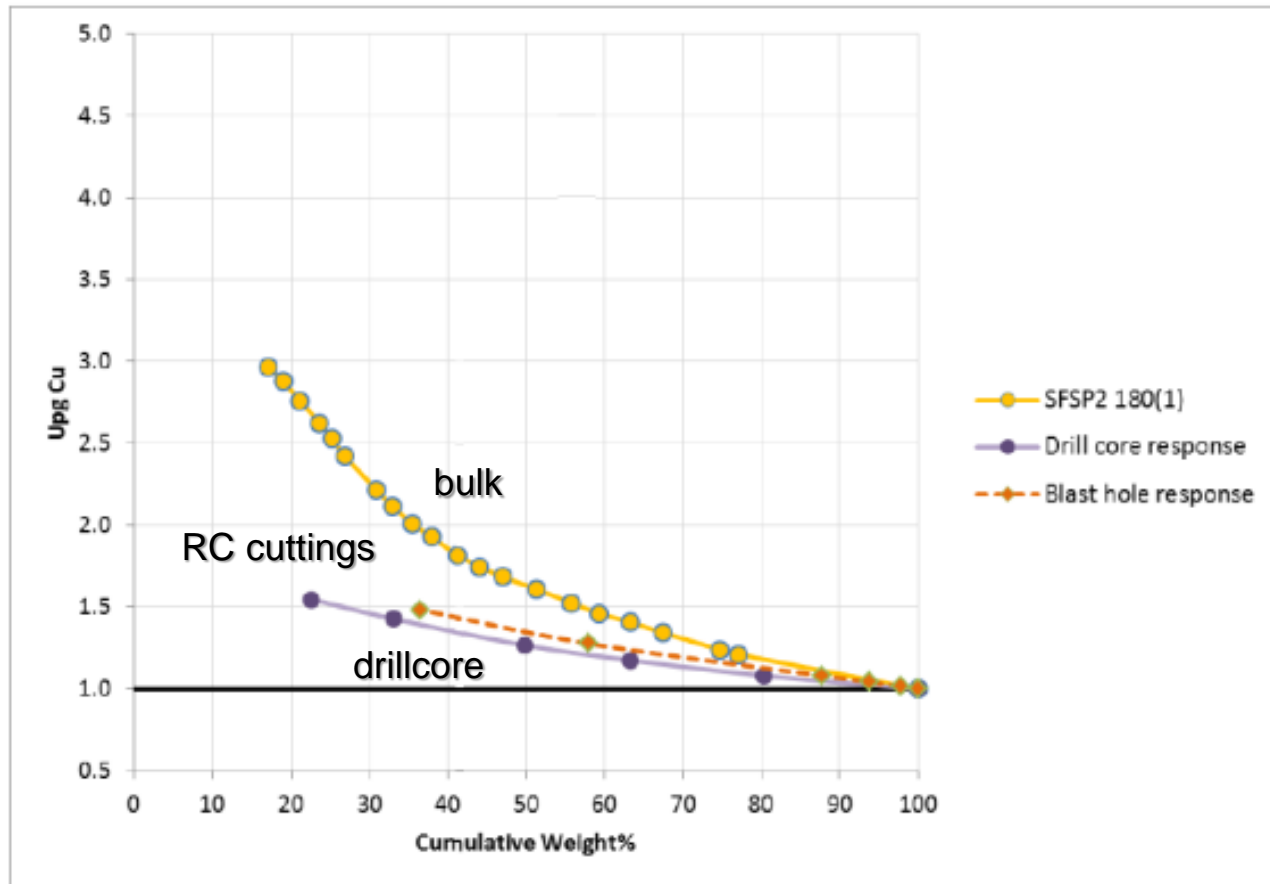
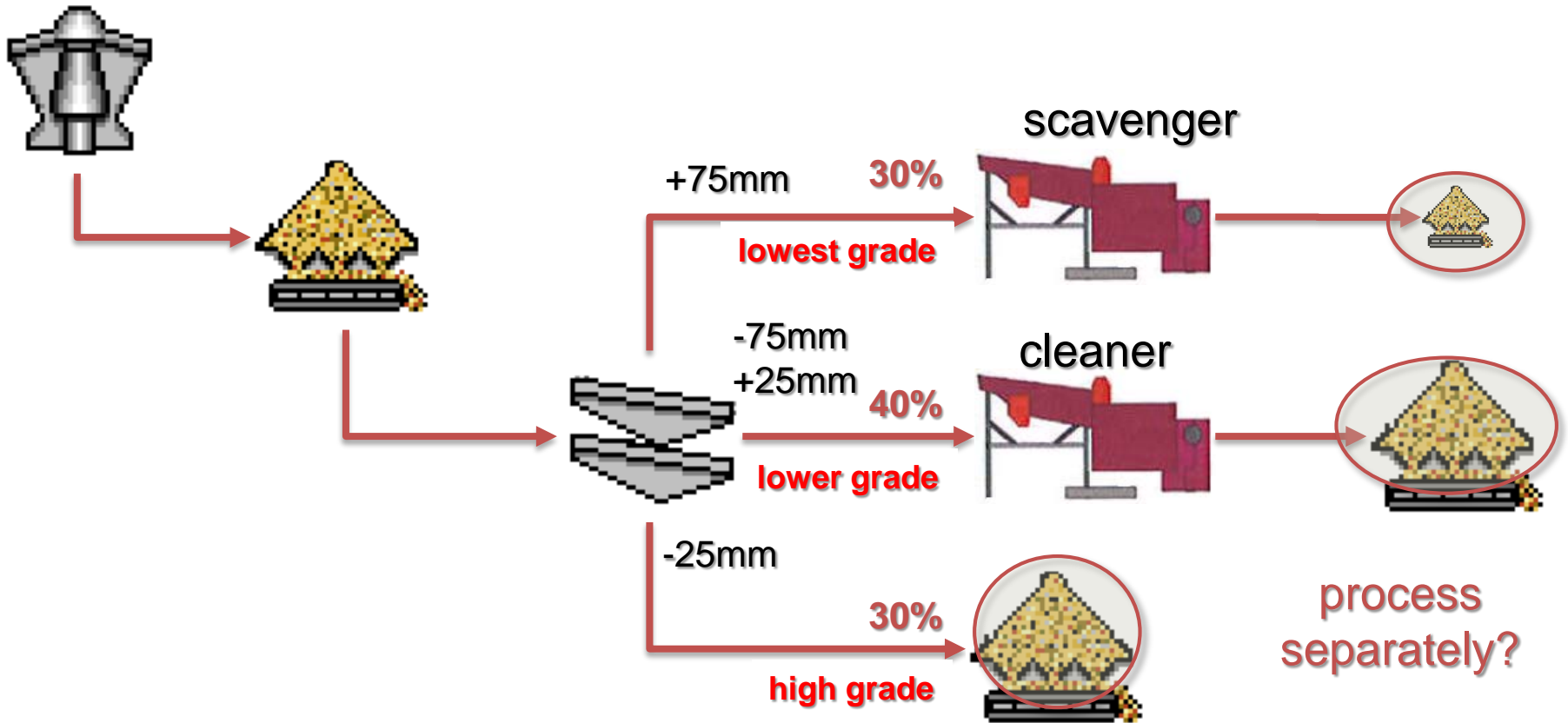


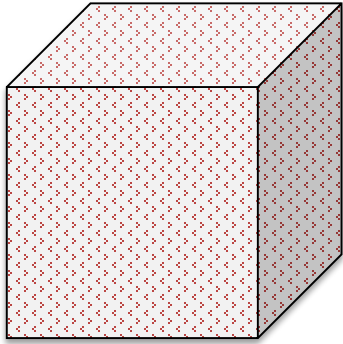
Figure 19. Upgrade Cu SF SP2 180 (1) bulk sample and the blast hole and drill core response related.

*"Development of Geometallurgical Laboratory Tests to Characterize Metal Pre-concentration by Size", Carrasco, C., Keeney, L. & Walters, S. IMPC 2014*

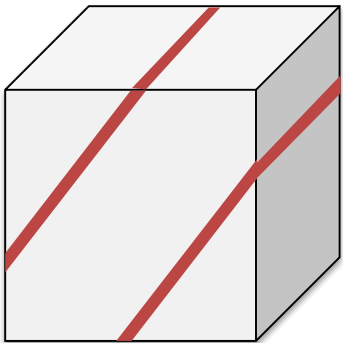
# Example flowsheet (involving ore sorters)



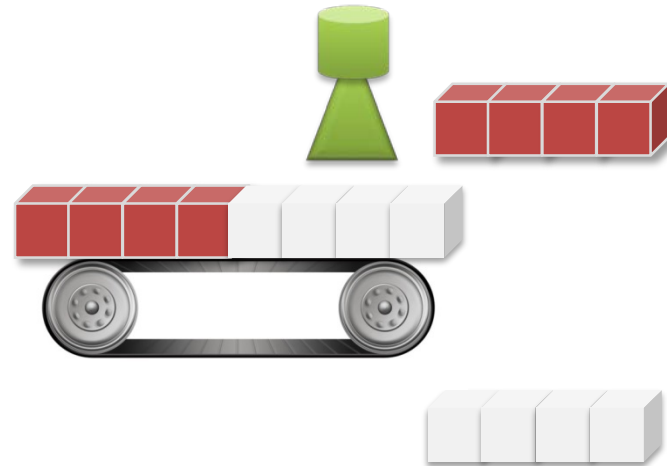
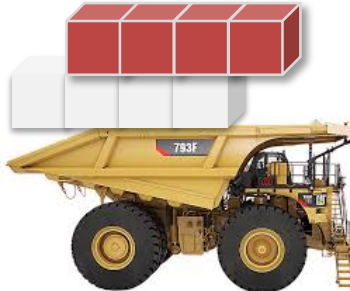
# Bulk/particle concentration



Homogenous



Heterogeneous

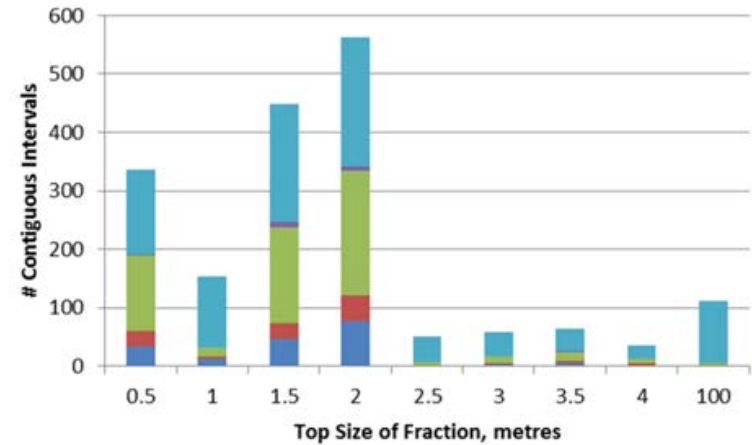


# Heterogeneity assessment

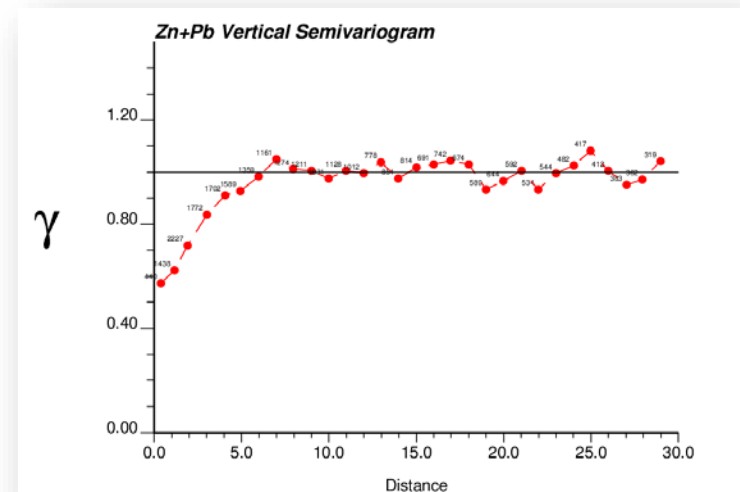
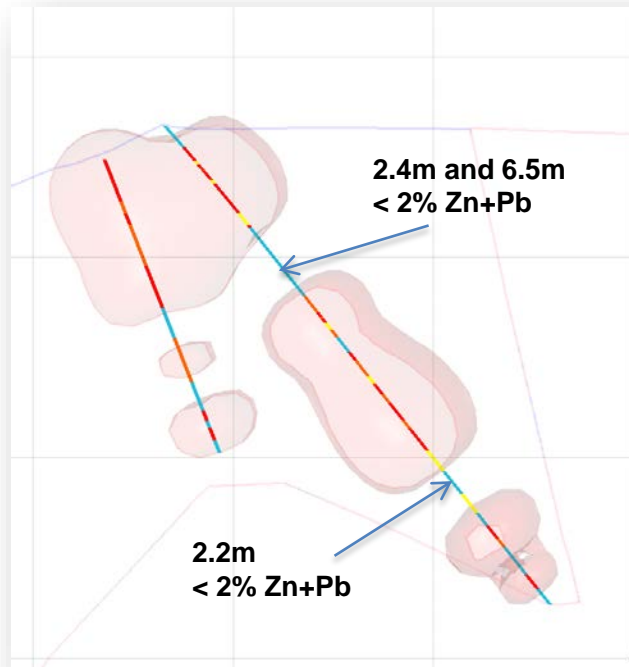
## Analysis of drillcore assays

## Spatial assessment

### Distribution of Waste Contiguous Intervals



## Variograms



# Summary

## Facing more challenging mill feed

- ⇒ lower grade, harder, more complex
- ⇒ is all of it worth processing?
- ⇒ should some of it be separated, deferred or returned to the source?

## Options

- ⇒ upgrade before it hits the grinding circuit
- ⇒ upgrade after it exits the AG/SAG mill

## What is the cost of 'optimal' metal recovery?

- ⇒ are we paying a high cost/low efficiency for maximum recovery?